# A MULTIPHASE MODEL FOR THE NUMERICAL SIMULATION OF ICE-FORMATION IN SEA-WATER

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**Abstract.** The first aim of this work is to improve the models currently available for the simulation of ice production in turbulent seawater, by means of the development of a multiphase model able to describe all the stages of ice production, overcoming the limitation of previous attempts, mainly based on Boussinesq approximation. We consider the mixture of ice and seawater as a dense compressible fluid, and we model the behaviour of seawater by an equation of state that links seawater density to temperature, salinity and pressure. The model is able to reproduce the interaction phenomena occurring between phases when the ice volume fraction exceeds the values allowed by the Boussinesq approximation, including in the momentum equations additional terms, related to the drag force between liquid and particles, and to the particle-particle interaction force. The second aim of our work is to implement and validate a numerical solver of our model. For this purpose, the model uses a sophisticated modelling approach, typically adopted for the numerical simulation of multiphase flows of industrial interest. The multiphase model can be coupled to the Large Eddy Simulation technique. The behaviour of the governing equations in the incompressible limit is investigated by means of a low-Mach number asymptotic analysis. The divergence constraint condition for the velocity field of continuous phase can then been imposed on the zero-Mach number equations by means of a projection method. The governing equations are discretized using the finite volume method, and the performance of the multiphase model has been assessed by solving a laminar Rayleigh-Bénard convection, for both large and small ice concentration regimes. In small concentration regime, the numerical solutions have been compared with the solutions obtained by a finite difference numerical code, based on the Boussinesq approximation.

#### 1 INTRODUCTION

Ice formation in the ocean is a complex phenomenon, whose correct description is essential in order to model adequately the atmosphere-ocean heat fluxes, the salt rejection phenomena and the damping effects related to the interactions among ice production, salt rejection and turbulent convection. The first stage of ice formation at the supercooled free surface of oceans, rivers and lakes is denoted as frazil-ice, a suspension of small individual randomly-oriented crystals, typically of 1 - 4 mm in diameter and 1 -  $100~\mu$  m in thickness [28, 31]. The frazil ice evolves rapidly into a thin slurry of ice platelets, known as grease ice. As cooling continues, the crystals freeze together into small disks called pancake-ice. Finally, during the last stage of sea ice evolution, the pankace-ice coalesces into a continuous ice sheet.

In this work, we focus our attention on the initial stages of ice production, frazil and grease ice. It is well known that ice formation greatly affects the geophysical and biological processes occurring in the polar oceans and that the subsequent salt rejection could play an important role in stimulating the convection processes in the oceans. Moreover, the presence of ice particles in rivers could produce serious damages to hydroelectric facilities, such as the blocking of turbine intakes, or the blockage of hydroelectric reservoirs. Therefore, the experimental and mathematical investigation of ice production has become, during the years, an active field of research.

The aim of this work is to improve the models currently available for the simulation of ice production in turbulent seawater, by means of the development of a multiphase model able to describe all the stages of ice production, overcoming the limitation of previous attempts, see e.g. [36, 42, 24, 40, 41, 21], mainly based on Boussinesq-like approximation. More specifically, in this work we consider the mixture ice-sea water as a dense compressible fluids. We model the behaviour of seawater by means of an equation of state derived from [7], that links seawater density to temperature, salinity and pressure, allowing us to go beyond the Boussinesq approximation. The model is able to reproduce the interaction phenomena occurring between phases when ice volume fraction is large, including in the momentum equations additional terms, related to the drag force between liquid and particles, and to the particle-particle interaction force. For this purpose, the model uses a sophisticated modelling approach, typically adopted for the numerical simulation of multiphase flows of industrial interest [16]. A low-Mach number asymptotic analysis has been performed to investigate the behaviour of the multiphase equations in the incompressible limit. The divergence constraint condition for the velocity field of continuous phase can then been imposed on the zero-Mach number equations by means of a projection method. As a starting point toward the development of an advanced numerical solver implementing our multiphase model, we develop a finite volume solver by means of a projection method based on [4, 19, 20], to be valid under the Boussinesq approximation, i.e. for small ice concentration regime, using the OpenFOAM library.

The paper is organized as follows: section 2 describes the multiphase model equations for the mixture ice-seawater, the non-dimensional form and the asymptotic analysis, whereas section 3 is devoted to the Boussinesq model equations. In section 4 we present the time discretization by projection method, for the Boussinesq model. Section 5 is devoted to the numerical results for a Boussinesq laminar Rayleigh-Bénard convection, for water and for the mixture ice-water, and ice-salt-water.

#### 2 THE MULTIPHASE MODEL EQUATIONS

We now introduce the multiphase model equations according to the Eulerian-Eulerian approach, coupled with a sophisticated modelling approach for the interaction terms between phases, typically adopted for the numerical simulation of multiphase flows of industrial interest. The governing equations proposed here have been derived carrying out a volume averaging considering an averaging volume V such as  $l^3 \ll V$ , where l denotes the mean distance between the ice particles. We define the density of the mixture ice-seawater as  $\rho = \phi_I \rho_I + (1-\phi_I) \rho_W$ , in which  $\phi_I$  stands for the ice volume fraction, and  $\rho_I$  and  $\rho_W$  denote the ice and water density, respectively. In this work we consider the ice density as a constant value. A large number of models for the equation of state for seawater have been proposed over the years in the oceanographic literature. We have focused our attention on those formulations suitable for numerical modelling, see e.g.[6, 15, 14, 33, 32, 29, 23]. Here we propose a reduced form for the equation of state, derived from the equation proposed in [7], that combines the approaches proposed in [15, 23], providing a simplification of the UNESCO formula [33] that has been found to be valid for  $-2^{\circ}C < \theta < 40^{\circ}C$ ,  $0 \ psu < S < 42 \ psu$ . Our state equation can be written as

$$\rho_{W}(T, S, p) = D_{r}p + E_{r},\tag{1}$$

where the  $D_r$  and  $E_r$  coefficients stand for  $D_r = b_5 T S + b_2 T + b_1$ , and  $E_r = a_5 T S + a_4 T^2 + a_3 S + a_2 T + a_1 + \rho_0$ ,  $\rho_0 = 1000 kg/m^3$  is a reference density. The coefficients  $a_i$  and  $b_i$  are given in Table 1. According to the equation 1, the speed of sound is given by  $c = \left[1/D_r\right]^{1/2}$ .

n	$a_n$	$b_n$
1	$-9.20601 \times 10^{-2}$	$+5.07043 \times 10^{-1}$
2	$+5.10768 \times 10^{-2}$	$-3.69119 \times 10^{-3}$
3	$+8.05999 \times 10^{-1}$	-
4	$-7.40849 \times 10^{-3}$	-
5	$-3.01036 \times 10^{-3}$	$+1.75145 \times 10^{-5}$

Table 1: Coefficients of the equation of state

The continuity equations for the liquid and solid phases can be written as

$$\frac{\partial}{\partial t}[(1 - \phi_I)\rho_W] + \frac{\partial}{\partial x_i}[(1 - \phi_I)\rho_W u_i] = S_{mass}, \tag{2}$$

$$\frac{\partial}{\partial t} \left( \phi_{I} \rho_{I} \right) + \frac{\partial}{\partial x_{i}} \left( \phi_{I} \rho_{I} v_{i} \right) = -S_{mass}. \tag{3}$$

where  $S_{mass}$  is the source term, defined as

$$S_{mass} = \frac{2\phi_{\rm I}h}{RL} \left( T_f - T_{\rm w} \right),\tag{4}$$

where h is the convective heat transfer coefficient, R stands for the average radius of the ice particles, L is the specific latent heat of fusion,  $T_{\rm w}$  denotes the water temperature and  $T_f$  is the freezing temperature. The momentum equations for water and ice read

$$\frac{\partial}{\partial t} \left[ (1 - \phi_I) \rho_W u_i \right] + \frac{\partial}{\partial x_j} \left[ (1 - \phi_I) \rho_W u_j u_i \right] + f_{i,j}^{cor} u_j = -(1 - \phi_I) \frac{\partial \bar{p}}{\partial x_i} + (1 - \phi_I) \frac{\partial \tau_{ij}}{\partial x_j} + F_i^W + (1 - \phi_I) \bar{\rho}_W g_i + S_{mom}, \quad (5)$$

$$\frac{\partial}{\partial t} \left( \phi_{I} \rho_{I} v_{i} \right) + \frac{\partial}{\partial x_{j}} \left( \phi_{I} \rho_{I} v_{j} v_{i} \right) + f_{i,j}^{cor} v_{j} = -\phi_{I} \frac{\partial \bar{p}}{\partial x_{i}} + \phi_{I} \frac{\partial \tau_{ij}}{\partial x_{j}} + F_{i}^{I} + \phi_{I} \rho_{I} g_{i} - S_{mom}, \tag{6}$$

where the quasi pressure  $\bar{p}$  is defined as  $\bar{p}=p+\rho_0gz$ , and  $\bar{\rho}_w$  stands for  $\bar{\rho}_w=\rho-\rho_0$ .  $F_i^w$  and  $F_i^I$  can be split in two terms  $F_i^w=f_i^{w,drag}+f_i^{w,I}$  and  $F_i^I=f_i^{I,drag}+f_i^{I,I}$ . Here,  $f_i^{w,drag}$  and  $f_i^{I,drag}$  denote the drag terms between seawater and particles, depending on the relative velocity  $(u_i-v_i)$ ;  $f_i^{w,I}$  denotes the shear stress term, analogous to the Reynolds stress in a single phase flow, that accounts for the velocity deviations that can occur on the seawater flow around a single particle;  $f_i^{I,I}$  denotes the particle-particle interaction term.  $S_{mom}$  is the source term and  $f_{i,j}^{cor}$  is an antisymmetric tensor such that  $f_{i,j}^{cor}u_j$  and  $f_{i,j}^{cor}v_j$  represent the Coriolis rotational forces on water and ice, respectively.

The momentum source term can be expressed as

$$S_{mom} = \frac{2\phi_{\rm I}h}{RL} \left( T_f - T_{\rm W} \right) v_i. \tag{7}$$

The liquid-solid drag term satisfies  $f_i^{w,drag} = -f_i^{I,drag}$ . Following the approach proposed in [17], for gas-solid fluidized bed,  $f_i^{w,drag}$  can be written as  $f_i^{w,drag} = K_D (u_i - v_i)$ , where  $K_D$  stands for the two-phase drag coefficient. For the evaluation of  $K_D$  we refer to [17], in which  $K_D$  is defined as a function of a drag coefficient  $C_D$ , and the relative Reynolds number  $Re_s = (\rho_w D \mid v_i - u_i \mid)/\mu_w$ . A large number of models have been proposed during the years for the evaluation of the drag terms, see e.g. [43], for gas-solid multiphase flows, and [17, 43, 45], for the evaluation of the liquid-solid drag in the framework of pipeline slurry flows, fluidized bed reactors, as well as in other chemical reacting systems, see e.g. [27, 22, 39, 46, 11, 37], or in numerical modelling of volcanic eruptions, see e.g. [8, 9]. The term  $f_i^{w,I}$  is analogous to the Reynolds stress in a single phase flow. Following the approach reported in [12], we can define  $f_i^{w,I}$  by means of an effective stress  $\tau_{ij}^e$  such that

$$f_i^{W,I} = \frac{\partial}{\partial x_j} \left( (1 - \phi_I) \, \tau_{ij}^e \right), \tag{8}$$

where the effective shear stress,  $\tau_{ij}^e$ , is related to the turbulence parameters of the flow. The evaluation of  $\tau_{ij}^e$ , is often carried out by means of eddy viscosity models. The particle-particle interaction term can be written as,

$$f_i^{I,I} = \phi_I \frac{\partial}{\partial x_j} \left( -p_s \delta_{ij} + \tau_{s,ij} \right). \tag{9}$$

The terms  $p_s$  and  $\tau_{s,ij}$  stand for the solid pressure and the solid shear stress tensor, respectively.  $p_s$  and  $\tau_{s,ij}$  can be evaluated as function of the granular temperature  $\Theta$ , according to the kinetic theory, originally applied by Bagnold [2] to this purpose. Starting from [2], several efforts have been devoted over the years to the development of the kinetic theory, see e.g [35, 38, 30, 26]. Here we mainly refer to the formulations proposed in [16, 30, 25]. Following this theory, an additional transport equation for the kinetic energy of the fluctuating motion of the dispersed phase, also called granular temperature  $\Theta$ , is required. The kinetic energy associated with the particle velocity fluctuation, can be expressed as  $\Theta = \frac{1}{3}\langle C \rangle^2$ , where C is the deviation of the particle velocity from the mean velocity. The operator  $\langle \ \rangle$  denotes the mean value based on the Gaussian distribution. The equation for the granular temperature can be written, following [16], as

$$\frac{3}{2} \left[ \frac{\partial}{\partial t} \left( \rho_{I} \phi_{I} \Theta \right) + \frac{\partial}{\partial x_{i}} \left( \rho_{I} \phi_{I} v_{i} \Theta \right) \right] = \left[ -p_{s} \delta_{ij} + \tau_{s,ij} \right] \frac{\partial v_{i}}{\partial x_{j}} - \frac{\partial}{\partial x_{i}} \left( k_{\Theta} \frac{\partial \Theta}{\partial x_{i}} \right) - \Gamma_{\Theta}. \tag{10}$$

Here,  $p_s$ ,  $\tau_{s,ij}$ ,  $k_{\theta}$ ,  $\Gamma_{\theta}$  stand for the solid pressure, the solid shear stress tensor, the coefficient of conductivity of granular temperature, and the dissipation term, respectively, and can be calculated as functions of  $\Theta$  using different approaches, see e.g. [30, 16, 44, 25].

The transport equation for the water temperature can be written as follows

$$\frac{\partial}{\partial t} \left[ (1 - \phi_{I}) T_{W} \right] + \frac{\partial}{\partial x_{i}} \left[ (1 - \phi_{I}) u_{i} T_{W} \right] = \frac{\partial}{\partial x_{i}} \left( (1 - \phi_{I}) k_{t} \frac{\partial T_{W}}{\partial x_{i}} \right) + \phi_{I} \lambda_{t} \left( T_{I} - T_{W} \right) + S_{T}.$$
(11)

The parameter  $\lambda_t$  is defined as  $\lambda_t = \frac{3h}{c_n \rho_W R}$ .  $S_T$  is the source term, defined as

$$S_T = \frac{2h\phi_I}{Rc_p\rho_W} \left( T_f - T_W \right), \tag{12}$$

where  $c_p$  stands for the water specific heat at constant pressure.

The equation for the salinity S is formulated as

$$\frac{\partial}{\partial t} \left[ (1 - \phi_{I}) S \right] + \frac{\partial}{\partial x_{i}} \left[ (1 - \phi_{I}) S u_{i} \right] = \frac{\partial}{\partial x_{i}} \left( (1 - \phi_{I}) k_{s} \frac{\partial S}{\partial x_{i}} \right) + S_{sal}, \tag{13}$$

where  $k_s$  is the salt diffusivity, and  $S_{sal}$  is the source term,

$$S_{sal} = \frac{2hS_v\phi_I\rho_I}{RL\rho_W} \left(T_f - T_W\right),\tag{14}$$

where  $S_v$  denotes the increase of salinity due to the freezing, that can be defined as  $S_v=m_s/\left[V\left(1-\frac{\phi_I\rho_I}{\rho}\right)\right]$ , in which  $m_s$  stands for the salt mass and V is the volume of the water-ice mixture.

### 2.1 Non-dimensional form

In order to obtain the non-dimensional form of the governing equations, we consider the vertical length of the computational domain L as the reference length; the temperature gap between upper and lower boundary of the computational domain,  $\Delta T$ , as temperature scale; the water velocity  $u_{\infty}$ , as the velocity scale; the characteristic time  $t^*$  as temporal scale; the water density,  $\rho_{w_{\infty}}$ , as density scale; and  $p_{\infty}$  and  $S_0$ , as reference pressure and reference salinity, respectively. We define the following dimensionless parameters,

$$\widetilde{\alpha} = \alpha \Delta T, \ \widetilde{S} = \frac{S}{S_0 \alpha \Delta T}, \ \widetilde{\Theta} = \frac{\Theta}{u_\infty^2}, \ \widetilde{p}_s = \frac{p_s}{\rho_{w_\infty} u_\infty^2}, \ M_\infty = \frac{u_\infty}{c_\infty},$$
 (15)

and the f parameter as  $f=u_\infty t^*/L$ . For simplicity, in the following sections we denote  $S_0 \alpha \Delta T$  as  $S_\infty$ , and  $\Delta T$  as  $T_\infty$ . Other dimensionless parameters are the non-dimensional numbers, Reynolds,  $R_e$ , Prandtl,  $P_r$ , Rayleigh,  $R_a$ , and Schmidt,  $S_{c_s}$ 

$$R_e = \frac{u\rho_w L}{\mu}, \ P_r = \frac{\nu}{k_t}, \ R_a = \frac{g\alpha L^3 \Delta T}{k_t \nu}, \ S_{c_s} = \frac{\nu}{k_s},$$
 (16)

where  $\mu$  and  $\nu$  are the dynamic and kinematic viscosity, respectively,  $k_t$  is the water thermal diffusivity,  $\alpha$  the thermal expansion coefficient, g the gravity acceleration and  $k_s$  is the salt diffusivity. The non-dimensional form of the equation of state, Equation 1, yields

$$\widetilde{\rho}_{\mathbf{w}} = D_r^* \widetilde{D}_r \widetilde{p} + E_r^* \widetilde{E}_r, \tag{17}$$

$$D_r^* = \frac{D_{r_{\infty}} p_{\infty}}{\rho_{w_{\infty}}}, \ E_r^* = \frac{E_{r_{\infty}}}{\rho_{w_{\infty}}}, \ \widetilde{D}_r = \frac{D_r}{D_{r_{\infty}}}, \ \widetilde{E}_r = \frac{E_r}{E_{r_{\infty}}}.$$
 (18)

In the following we will work with the non dimensional equations, dropping the sign for simplicity. The non-dimensional mass conservation equations can be written as,

$$\frac{\partial}{\partial t} \left[ (1 - \phi_{I}) \, \rho_{W} \right] + f \frac{\partial}{\partial x_{i}} \left[ (1 - \phi_{I}) \, \rho_{W} u_{i} \right] = S_{mass}, \tag{19}$$

$$\frac{\partial}{\partial t} \left( \phi_{I} \rho_{I} \right) + f \frac{\partial}{\partial x_{i}} \left( \phi_{I} \rho_{I} v_{i} \right) = -S_{mass}, \tag{20}$$

where the source term yields,

$$S_{mass} = \frac{2\phi_I h t^*}{R L \rho_{w_{res}}} \left( T_f - T_w \right). \tag{21}$$

The non-dimensional momentum equations can be defined as

$$\begin{split} \frac{\partial}{\partial t} \left[ \left( 1 - \phi_{\rm I} \right) \rho_{\rm W} u_i \right] + f \frac{\partial}{\partial x_j} \left[ \left( 1 - \phi_{\rm I} \right) \rho_{\rm W} u_j u_i \right] + f_{Cor} u_i &= -f \frac{p_{\infty}}{\rho_{\rm W_{\infty}} c_{\infty}^2} \frac{1}{M_{\infty}^2} \left( 1 - \phi_{\rm I} \right) \frac{\partial \bar{p}}{\partial x_i} + f \frac{1}{Re_{\infty}} \left( 1 - \phi_{\rm I} \right) \left( \frac{\partial^2 u_j}{\partial x_j \partial x_i} + \frac{1}{3} \frac{\partial}{\partial x_j} \left( \frac{\partial u_i}{\partial x_i} \right) \right) + F_i^{\rm W} + f \frac{R_a}{P_r Re_{\infty}^2 \alpha} \left( 1 - \phi_{\rm I} \right) \bar{\rho}_{\rm W} - S_{mom}, (22) \end{split}$$

$$\frac{\partial}{\partial t} \left( \phi_{I} \rho_{I} v_{i} \right) + f \frac{\partial}{\partial x_{j}} \left( \phi_{I} \rho_{I} v_{j} v_{i} \right) + f_{Cor} v_{i} = -f \frac{p_{\infty}}{\rho_{W_{\infty}} c_{\infty}^{2}} \frac{1}{M_{\infty}^{2}} \phi_{I} \frac{\partial \bar{p}}{\partial x_{i}} + f \frac{1}{Re_{\infty}} \phi_{I} \left( \frac{\partial^{2} u_{j}}{\partial x_{j} \partial x_{i}} + \frac{1}{3} \frac{\partial}{\partial x_{j}} \left( \frac{\partial u_{i}}{\partial x_{i}} \right) \right) + F_{i}^{I} + f \frac{R_{a}}{P_{r} Re_{\infty}^{2}} \alpha \phi_{I} \rho_{I} + S_{mom}, \tag{23}$$

where the source term stands for

$$S_{mom} = \frac{2\phi_I h t^*}{RL\rho_{w_{\infty}}} \left( T_f - T_w \right) v_i. \tag{24}$$

The temperature equation for water can be written as

$$\frac{\partial}{\partial t} \left[ (1 - \phi_{I}) T_{W} \right] + f \frac{\partial}{\partial x_{i}} \left[ (1 - \phi_{I}) u_{i} T_{W} \right] = \frac{t^{*} \nu}{L^{2}} \frac{\partial}{\partial x_{i}} \left( (1 - \phi_{I}) \frac{1}{P_{r}} \frac{\partial T_{W}}{\partial x_{i}} \right) + \phi_{I} t^{*} \lambda_{t} \left( T_{I} - T_{W} \right) + S_{T}.$$

$$(25)$$

The source term is given by

$$S_T = \frac{2ht^*\phi_I}{Rc_p\rho_w\rho_{w_\infty}} \left(T_f - T_w\right). \tag{26}$$

The non-dimensional transport equation for salinity can be written as,

$$\frac{\partial}{\partial t} \left[ (1 - \phi_{I}) S \right] + f \frac{\partial}{\partial x_{i}} \left[ (1 - \phi_{I}) S u_{i} \right] = f \frac{\partial}{\partial x_{i}} \left( (1 - \phi_{I}) \frac{1}{ScRe_{\infty}} \frac{\partial S}{\partial x_{i}} \right) + S_{sal}, \tag{27}$$

$$S_{sal} = \frac{2ht^*S_v\phi_I\rho_I\rho_{W_{\infty}}}{RLS_{\infty}\rho_W} \left(T_f - T_W\right). \tag{28}$$

Finally, for granular temperature, the non dimensional form yields,

$$\frac{3}{2} \left[ \frac{\partial}{\partial t} \left( \rho_{I} \phi_{I} \Theta \right) + f \frac{\partial}{\partial x_{i}} \left( \rho_{I} \phi_{I} v_{i} \Theta \right) \right] = \left[ -f p_{s} \delta_{ij} + \tau_{s,ij} \right] \frac{\partial v_{i}}{\partial x_{j}} - \frac{\partial}{\partial x_{i}} \left( k_{\Theta} \frac{\partial \Theta}{\partial x_{i}} \right) - \Gamma_{\Theta}. \tag{29}$$

### 2.2 Low-Mach number asymptotic analysis

To investigate the behaviour of the multiphase equations in the incompressible limit, we have expanded each flow variables as e.g., the pressure,

$$p(x, t, M_{\infty}) = p^{(0)} + M_{\infty}^{2} p^{(2)}(x, t, M_{\infty}).$$
(30)

For simplicity, here we report only the zero-Mach number equation for seawater density, Equation 17, the zero-Mach number equation for mass concentration, Equation 19, and the leading and the zero-order equations for momentum, Equations 22 and . The other zero-Mach number equations follow the non-dimensional representation, with all the variables evaluated at the zero-order. The non-dimensional equation for seawater density, at order  $O\left(M_\infty^0\right)$ , is derived as:

$$\rho_w^{(0)} = D_r^* \left( D_r^{(0)} p^{(0)} \right) + E_r^* E_r^{(0)}, \tag{31}$$

where the coefficients  $D_r^{(0)}$  and  $E_r^{(0)}$  are functions of the zero-order temperature and salinity, see the Appendix A for the detailed expression of each coefficient. The water mass conservation at order  $O\left(M_\infty^0\right)$  yields

$$\frac{\partial}{\partial t} \left[ \left( 1 - \phi_I^{(0)} \right) \rho_W^{(0)} \right] + f \frac{\partial}{\partial x_i} \left[ \left( 1 - \phi_I^{(0)} \right) \rho_W^{(0)} u_i^{(0)} \right] = S_{mass}^{(0)}. \tag{32}$$

The zero-order ice mass conservation is given similarly. The water and ice momentum equations at the leading order  $O\left(M_{\infty}^{-2}\right)$  yield

$$\frac{\partial \bar{p}^{(0)}}{\partial x_i} = 0, (33)$$

therefore, according to the definition of quasi-pressure  $\bar{p}^{(0)}$ , we obtain

$$\frac{\partial p^{(0)}}{\partial x} = \frac{\partial p^{(0)}}{\partial y} = 0,\tag{34}$$

$$\frac{\partial p^{(0)}}{\partial z} = -\rho_0 g. \tag{35}$$

The water momentum equation at order  $O\left(M_{\infty}^{0}\right)$  yields:

$$\frac{\partial}{\partial t} \left[ \left( 1 - \phi_{I}^{(0)} \right) \rho_{W}^{(0)} u_{i}^{(0)} \right] + f \frac{\partial}{\partial x_{j}} \left[ \left( 1 - \phi_{I}^{(0)} \right) \rho_{W}^{(0)} u_{j}^{(0)} u_{i}^{(0)} \right] + f_{Cor}^{(0)} u_{i}^{(0)} =$$

$$- f \frac{p_{\infty}}{\rho_{W_{\infty}} c_{\infty}^{2}} \left( 1 - \phi_{I}^{(0)} \right) \frac{\partial \bar{p}^{(2)}}{\partial x_{i}} + f \frac{1}{Re_{\infty}} \left( 1 - \phi_{I}^{(0)} \right) \left( \frac{\partial^{2} u_{j}^{(0)}}{\partial x_{j} \partial x_{i}} + \frac{1}{3} \frac{\partial}{\partial x_{j}} \left( \frac{\partial u_{i}^{(0)}}{\partial x_{i}} \right) \right) +$$

$$F_{i}^{W(0)} + f \frac{R_{a}}{P_{r} R_{e_{\infty}}^{2}} \alpha \left( 1 - \phi_{I}^{(0)} \right) \bar{\rho}_{W}^{(0)} - S_{mom}^{(0)}. \tag{36}$$

The ice momentum equation at order  $O\left(M_{\infty}^{0}\right)$  can be similarly derived. Using the continuity equation, Equation 32, and assuming f=1, the following constraint on the divergence of the water velocity is obtained

$$\nabla \cdot u_i^{(0)} = \frac{1}{\left(1 - \phi_I^{(0)}\right) \rho_W^{(0)}} \left[ -\frac{D}{Dt} \left(1 - \phi_I^{(0)}\right) \rho_W^{(0)} + S_{mass}^{(0)} \right],\tag{37}$$

where  $\frac{D}{Dt} \left( 1 - \phi_{\rm I}^{(0)} \right) \rho_{\rm W}^{(0)}$  can be written as

$$\frac{D}{Dt} \left( 1 - \phi_I^{(0)} \right) \rho_w^{(0)} = \left( 1 - \phi_I^{(0)} \right) \frac{D \rho_w^{(0)}}{Dt} - \rho_w^{(0)} \frac{D \phi_I^{(0)}}{Dt}. \tag{38}$$

Using the zero-oder ice mass conservation,  $\frac{D\phi_I^{(0)}}{Dt}$  can be obtained as

$$\frac{D\phi_I^{(0)}}{Dt} = -\frac{S_{mass}^{(0)}}{\rho_I^{(0)}} - \phi_I^{(0)} \frac{\partial v_i^{(0)}}{\partial x_i},\tag{39}$$

and  $\frac{D\rho_W^{(0)}}{Dt}$  can be derived as

$$\frac{D\rho_{\mathbf{w}}^{(0)}}{Dt} = \frac{\partial\rho_{\mathbf{w}}^{(0)}}{\partial S^{(0)}} \bigg|_{T_{\mathbf{w}}^{(0)}, p^{(0)}} \frac{DS^{(0)}}{Dt} + \frac{\partial\rho_{\mathbf{w}}^{(0)}}{\partial T_{\mathbf{w}}^{(0)}} \bigg|_{S^{(0)}, p^{(0)}} \frac{DT_{\mathbf{w}}^{(0)}}{Dt} + \frac{\partial\rho_{\mathbf{w}}^{(0)}}{\partial p^{(0)}} \bigg|_{T_{\mathbf{w}}^{(0)}, S^{(0)}} \frac{Dp^{(0)}}{Dt}, \tag{40}$$

in which all the partial derivative can be evaluated by means of the equation of state, whereas  $\frac{DS^{(0)}}{Dt}$  and  $\frac{DT_W^{(0)}}{Dt}$  can be derived using the zero-order temperature and salinity equations, respectively, and  $\frac{Dp^{(0)}}{Dt}$  can be evaluated considering the Equation 33, see the Appendix A for the complete derivation of these terms. The divergence constraint can then be rewritten as

$$\nabla \cdot u_i^{(0)} = \frac{1}{\left(1 - \phi_I^{(0)}\right) \rho_w^{(0)}} \left( -\phi_I^{(0)} \frac{\partial v_i^{(0)}}{\partial x_i} + \frac{1}{\rho_w^{(0)}} \left(1 - \frac{\rho_w^{(0)}}{\rho_I}\right) S_{mass}^{(0)} \right) - \frac{1}{\rho_w^{(0)}} \frac{D\rho_w^{(0)}}{Dt}. \tag{41}$$

The zero-order equations coupled with the divergence constraint, Equation 41, can then be discretized in time using a projection method, and the divergence constraint will be used to enforce the mass conservation and the equation of state.

#### 3 BOUSSINESQ APPROXIMATION OF THE MULTIPHASE MODEL EQUATIONS

Here we present the Boussinesq approximation for the multiphase equations introduced in the previous sections. This is a starting point for the development of a finite volume multiphase solver, based on the aforementioned multiphase model. The Boussinesq approximation, indeed, allows us to model the initial stage of the ice production phenomena, frazil-ice, in which the ice volume fraction typically does not exceed  $10^{-3}$ . The formulation reported here follows the approach presented in [1]. According to the Boussinesq approximation, the seawater density can be expressed by means of the following linearized equation of state, see e.g. [21]

$$\rho_{W} = \rho_{0} \left( 1 - \beta \left( T - T_{0} \right) + \beta_{s} \left( S - S_{0} \right) \right), \tag{42}$$

in which  $\rho_0$ ,  $T_0$ ,  $S_0$ , denote the reference density, temperature, and salinity, respectively, whereas  $\beta$  and  $\beta_s$  are the expansion coefficients. Using the Boussinesq approximation, density variations are sufficiently small such that they can be retained only in the buoyancy term of the momentum equation, see e.g [10]. According to such approximation, our multiphase model reduces to a single-phase model, then all the interaction terms and the mass and momentum source terms vanish. Retaining only the equations for water, and assuming the water density to be constant, except in the buoyancy term, the governing equations reduce to

$$\frac{\partial u_i}{\partial x_i} = 0, (43)$$

$$\frac{\partial u_i}{\partial t} + \frac{\partial \left(u_i u_j\right)}{\partial x_i} = -\frac{\partial \pi}{\partial x_i} + \frac{1}{Re} \frac{\partial^2 u_i}{\partial x_i^2} - g_i \left(\beta \left(T - T_0\right) - \beta_s \left(S - S_0\right)\right),\tag{44}$$

$$\frac{\partial T_{w}}{\partial t} + \frac{\partial (u_{i}T_{w})}{\partial x_{i}} = \frac{\partial}{\partial x_{i}} \left( k_{t} \frac{\partial T_{w}}{\partial x_{i}} \right) + S_{T}, \tag{45}$$

where  $\pi$  denotes the quasi-pressure, defined as  $\pi = (p - \rho_0 g)/\rho_0$ , according to the treatment proposed in [13]. The source term for temperature,  $S_T$ , is given by

$$S_T = \frac{2h}{Rc_p \rho_w \rho_I} \rho C_I \left( T_f - T_w \right), \tag{46}$$

where  $C_I$  denotes the ice mass concentration, and  $\rho$  stands for the density of the mixture, given by

$$\rho = \left(\frac{C_{\rm I}}{\rho_{\rm I}} + \frac{(1 - C_{\rm I})}{\rho_{\rm W}}\right)^{-1}.\tag{47}$$

We can describe the scalar transport phenomena for the ice mass concentration  $C_I$ , by means of the following equation

$$\frac{\partial}{\partial t} \left( \rho C_{I} \right) + \frac{\partial}{\partial x_{i}} \left( \rho C_{I} u_{i} \right) = -\omega_{r_{i}} \frac{\partial \left( \rho C_{I} \right)}{\partial x_{i}} + k_{I} \frac{\partial}{\partial x_{i}} \left( \rho \frac{\partial C_{I}}{\partial x_{i}} \right) + S_{C_{I}}, \tag{48}$$

where  $k_I$  is the ice thermal diffusivity, and  $S_{C_I}$  denotes the source term, that can be expressed as

$$S_{C_I} = \frac{2h}{RL\rho_I} \rho C_I \left( T_f - T_W \right). \tag{49}$$

The Equation 48 is derived assuming the ice velocity as  $u_I = u + \omega_r$ , where u is the velocity of the mixture, and  $\omega_r = (0, v_r, 0)$  stands for the rise velocity, related to buoyancy forces. In this

work we left  $\omega_r$  as a free parameter, to be evaluated according to experimental investigations, see e.g. [34]. The transport equation for salinity S can be written as

$$\frac{\partial S}{\partial t} + \frac{\partial}{\partial x_i} \left( S u_i \right) = \frac{\partial}{\partial x_i} \left( k_s \frac{\partial S}{\partial x_i} \right) + S_{sal}, \tag{50}$$

where  $k_s$  is the salt diffusivity, and  $S_{sal}$  is the source term, defined as follows

$$S_{sal} = \frac{2h}{RL\rho_{\rm w}} S_v \rho C_I \left( T_f - T_{\rm w} \right), \tag{51}$$

where the increase of salinity due to the freezing,  $S_v$ , stands for  $S_v = m_s/[V(1-C_I)]$ , in which  $m_s$  is the salt mass and V is the volume of the water-ice mixture.

#### 4 TIME DISCRETIZATION BY PROJECTION METHOD FOR BOUSSINESQ FLOWS

The Boussinesq simplification of the Navier-Stokes equations is integrated in time by a second order projection method constructed in order to have good kinetic energy conservation. Space discretization is performed by a cell-centered second order finite volume approach, while time evolution is computed by using the trapezoidal rule in a colocated non-incremental approximate projection method. The overall method is characterized by a limited amount of numerical dissipation, similarly to [19], and thus it forms an appropriate framework for developing future variants to be applied in direct and large-eddy simulations. An alternative projection approach for density variable flows is reported in [5]. Here we present only a brief overview of the numerical methodology, thus postponing a complete discussion of the projection method elsewhere.

The discretization of the evolution equations under the Boussinesq approximation involves several steps. All the primitive quantities are defined as cell averages at cell center of mass and at integer time steps, while only the quasi-pressure  $\pi$  is defined at cell centers and at half-times, similarly to [3]. Here we denote with  $A_f$  the area of cell faces, with  $n_{f,i}$  the face normal unit vector and with  $\overline{(\cdot)}^f$  the interpolation operator acting on cell centered quantities to construct face centered quantities.

Step 1. – The face normal velocities  $U^n=\overline{u_i^n}^f n_{f,i}$  are extrapolated in time using second order Adams-Bashforth

$$U^{n+1,\star} = \frac{3}{2}U^n - \frac{1}{2}U^{n-1},\tag{52}$$

which will be consistent with the incompressibility condition if the face normal velocities from the previous time steps are divergence-free. For the construction of the evolution equation for the ice concentration the face normal mass fluxes  $m^n = \overline{\rho^n}^f \overline{(u_i^n + \omega_{r,i})}^f n_{f,i}$  are constructed in a similar manner

$$m^{n+1,\star} = \frac{3}{2}m^n - \frac{1}{2}m^{n-1},\tag{53}$$

accordingly:

$$\rho^{n+1} = \frac{3}{2}\rho^n - \frac{1}{2}\rho^{n-1}. (54)$$

Step 2. – The temperature equation is integrated implicitly by the trapezoidal rule

$$\frac{T^{n+1} - T^n}{\Delta t} = -\frac{1}{2} \left[ D\left( U^{n+1,\star} \overline{T^{n+1}}^f \right) + D\left( U^{n+1,\star} \overline{T^n}^f \right) \right] + \frac{1}{2} \left[ L_{k_t}(T^{n+1}) + L_{k_t}(T^n) \right] + S_T^{n+1/2},$$
(55)

where we introduced the discrete second-order divergence operator D, approximating the divergence at cell centers from face centered quantities, and the discrete second order operator  $L_{k_t}$ , approximating  $\frac{\partial}{\partial x_i} \left( k_t \frac{\partial T}{\partial x_i} \right)$  at cell centers from cell centered quantities, in which we silently introduce the interpolation  $\overline{k_t}^f$ . This allows to construct the buoyancy terms in the other equa-

Step 3. – The salinity equation is integrated implicitly by the trapezoidal rule as well

$$\frac{S^{n+1} - S^n}{\Delta t} = -\frac{1}{2} \left[ D \left( U^{n+1,\star} \overline{S^{n+1}}^f \right) + D \left( U^{n+1,\star} \overline{S^n}^f \right) \right] + \frac{1}{2} \left[ L_{k_S}(S^{n+1}) + L_{k_S}(S^n) \right] + S_S^{n+1/2},$$
(56)

where the discrete operator  $L_{k_S}$  approximates  $\frac{\partial}{\partial x_i} \left( k_S \frac{\partial S}{\partial x_i} \right)$ . Successively the ice concentration equation is integrated by

$$\frac{\rho^{n+1}C^{n+1} - \rho^n C^n}{\Delta t} = -\frac{1}{2} \left[ D\left(m^{n+1,\star} \overline{C^{n+1}}^f\right) + D\left(m^{n+1,\star} \overline{C^n}^f\right) \right] + \frac{1}{2} \left[ L_{k_I \rho^{n+1}}(C^{n+1}) + L_{k_I \rho^n}(C^n) \right] + S_I^{n+1/2},$$
(57)

where the discrete operator  $L_{kI\rho^n}$  approximates  $\frac{\partial}{\partial x_j}\left(k_I\rho^n\frac{\partial C}{\partial x_j}\right)$  to second order accuracy. Step 4. – The momentum equation is integrated by the trapezoidal rule, thus obtaining a

predicted velocity field  $u_i^{n+1,\star}$  which is not generally divergence-free

$$\frac{u_i^{n+1,\star} - u_i^n}{\Delta t} = -\frac{1}{2} \left[ D\left( U^{n+1,\star} \overline{u_i^{n+1,\star}}^f \right) + D\left( U^{n+1,\star} \overline{u_i^n}^f \right) \right] 
+ \frac{1}{2} \left[ L_{\nu} \left( u_i^{n+1,\star} \right) + L_{\nu} \left( u_i^n \right) \right] - G_i \left( \pi^{n-1/2} \right) 
- \frac{1}{2} g_i \left[ \beta \left( \left( T^{n+1} - T_0 \right) + \left( T^n - T_0 \right) \right) - \beta_s \left( \left( S^{n+1} - S_0 \right) + \left( S^n - S_0 \right) \right) \right]$$
(58)

where we introduced the discrete second-order gradient operator  $G_i$  approximating the gradient at cell centers from cell centered quantities by the discrete Gauss theorem applied on  $\overline{\pi^{n-1/2}}^f$ . Step 5. – The term containing  $\pi^{n-1/2}$  is removed from the predicted velocity field

$$u_i^{n+1,\star\star} = u_i^{n+1,\star} + \Delta t \ G_i(\pi^{n-1/2})$$
 (59)

in order to construct a non-incremental projection step (i.e., a Poisson equation on  $\pi^{n+1/2}$  rather than on  $\pi^{n+1/2} - \pi^{n-1/2}$ ).

Step 6. – The Poisson equation is solved for the unknown  $\pi^{n+1/2}$  required to update the divergence-free face normal velocities

$$L\left(\pi^{n+1/2}\right) = \frac{1}{\Delta t} D\left(\overline{u_i^{n+1,\star\star}}^f\right). \tag{60}$$

Here homogeneous Neumann boundary conditions are applied to the discrete second order laplacian operator L, which are responsible for the preservation of the initial normal gradient of  $\pi^0$  at the boundaries (see, e.g., [18]).

Step 7. – The predicted and face normal velocities are respectively updated according to

$$u_i^{n+1} = u_i^{n+1,\star\star} - \Delta t \ G_i(\pi^{n+1/2}), \tag{61}$$

$$U^{n+1} = \left[ \overline{u_i^{n+1,\star\star}}^f n_{f,i} - \Delta t \ G_{n_f} \left( \pi^{n+1/2} \right) \right], \tag{62}$$

$$U^{n+1} = \left[ \overline{u_i^{n+1,\star\star}}^f n_{f,i} - \Delta t \ G_{n_f} \left( \pi^{n+1/2} \right) \right], \tag{62}$$

$$m^{n+1} = \left[ \overline{\rho^{n+1}}^f \left( \overline{u_i^{n+1,\star\star}} + \omega_{r,i} \right)^f n_{f,i} - \Delta t \ \overline{\rho^{n+1}}^f G_{n_f} \left( \pi^{n+1/2} \right) \right], \tag{63}$$

where the discrete second order face normal gradient operator  $G_{n_f}$  is introduced, approximating the normal gradient at cell faces from cell centered quantities. The resulting face normal velocities  $U^{n+1}$  are divergence-free as required by the convective terms. Tangential boundary conditions on  $u_i^{n+1}$  are now directly enforced, since they cannot result naturally from the projection step.

The initial value problem requires initial values of  $u_i^0$  at time t=0 and relative boundary conditions. In our calculations we always started from uniformly zero fields on  $u_i^0$  and  $\pi^0$ whenever possible, or we started from a velocity field resulting after an initial projection step. As a consequence we implicitly assumed at boundaries the artificial condition  $\frac{\partial \pi}{\partial x_i} n_{b,i} = 0$ , where  $n_{b,i}$  represents the unit vector normal to the boundary.

A numerical solvers called fsBMA has been implemented according to this formulation, by means of the OpenFOAM library [47].

#### **NUMERICAL RESULTS**

In order to validate the full multiphase model we shall proceed step by step. As a first step we consider here a simplified version of the equations, namely the Boussinesq approximation. The time discretization is the same described in the previous section, except for source terms, that have been integrated at first order for simplicity, and for the density of the mixture  $\rho$  that has been extrapolated at first order. Our analysis has to be intended as a sensitivity study of the influence of the ice formation process on the behaviour of the velocity and temperature fields, for unsalted and salted water, therefore does not completely reproduce the realistic condition of ice production in seawater. The results we present here are the numerical solutions of a three dimensional laminar Rayleigh-Bénard convection of a Boussinesq fluid. Numerical simulations have been performed using the developed fsBMA solver, for water, section 5.1, for the water-ice and water-ice-salt mixture, section 5.2.

#### **5.1** Laminar Rayleigh-Bénard convection for water

Numerical simulations have been performed for  $Ra = 2.3 \times 10^4$ , using a three dimensional 6DxDx6D domain, where D denotes the height, discretized by means of a uniform 60x10x60 computational grid and a non-uniform 60x50x60 grid, with the smaller mesh size near the top and bottom walls. The boundary conditions at top and bottom walls are freeslip for velocity. The zero-gradient condition has been imposed at top and bottom for pressure, whereas for the temperature we impose  $T_t$ , and  $T_b$ , respectively. The boundary conditions for all the lateral boundaries are periodic. The simulations have been carried out using  $T_t = 272.15 \, [K], \, T_b = 274.15 \, [K], \, {\rm and} \, \beta = 3.6476 \times 10^{-3} \, [1/K], \, \nu = 1.6438 \times 10^{-6} \, [m^2/s],$  $k_t = 1.3905 \times 10^{-7} \, [m^2/s]$  for the thermal expansion coefficient, kinematic viscosity coefficient, and thermal diffusivity, respectively. The simulations have been performed by imposing an initial random perturbation for the temperature and velocity fields. Numerical results have been compared with those obtained by means of a finite difference numerical code presented in [1], on a non-uniform 60x50x60 grid, locally refined near top and bottom walls.

Figure 1 shows the contours and the isolines for the temperature fields, and the  $U_y$  velocity component, in the vertical x, y midplane at z = 3D and in the horizontal x, z midplane, at y = D/2, respectively, obtained by means of the non-uniform 60x50x60 grid.

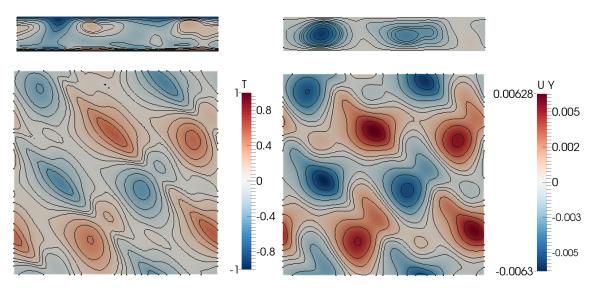


Figure 1: Contours and isolines of temperature, T, left column, and of the  $U_y$  velocity component, right column, in the x, y midplane, top row, and in the x, z midplane, bottom row, for water at  $Ra = 2.3 \times 10^4$ .

Figure 2 shows the comparison between the finite difference code, FD, and the developed finite volume solver fsBMA, in terms of the time average of the temperature profile, spatially averaged over the x, z plane, and the root mean square of  $U_y$  velocity profile, along the y axis.

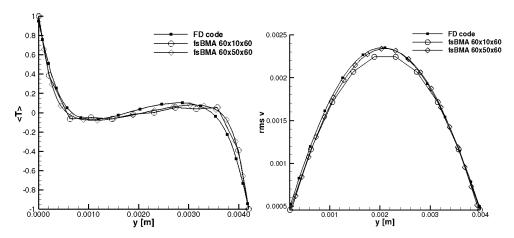


Figure 2: Comparison between the space-time average temperature profiles < T >, left plot, and between the root mean square of the  $U_y$  component, right plot, along the y axis, obtained with the FD code and the fsBMA solver.

The profiles in Figure 2 are referred to the 60x50x60 non-uniform mesh for the FD solver, and to the 60x10x60 and 60x50x60, uniform and non-uniform mesh, for the fsBMA solver. We observe that both the fsBMA space-time average profile < T >, and the root mean square of the  $U_y$  component are in good agreement with the FD results. Moreover, the comparison highlights the effects of the grid resolution. The finer non-uniform grid, indeed, allows us to obtain an

average temperature profile and a root mean square of  $U_y$  velocity that better reproduce the reference FD profile, suggesting a convergent trend of the curves increasing the grid resolution.

### 5.2 Laminar Rayleigh-Bénard convection for the ice-water and the ice-salt-water mixture

The numerical simulations have been carried out following the configuration adopted in the previous section, but now simulating the ice-water and the ice-water-salt mixture. Computations have been performed for both configurations on uniform 60x10x60 grid. We begin our analysis presenting the numerical results of the ice-water simulation. The simulation has been performed imposing on the top and bottom walls a zero gradient condition for the ice mass conservation. The rise velocity has been set  $w_r = 0.01m/s$ , according to the experimental investigation reported in [34], moreover the ice thermal diffusivity, the ice density and the particle average radius are,  $k_{\rm I}=1.18\times 10^{-6}\,[m^2/s]$ ,  $\rho_{\rm I}=917\,[kg/m^3]$ ,  $R=0.5\times 10^{-3}\,[m]$ , respectively, assuming the frazil-ice particles of disk-like shape. We perform the numerical simulation imposing an initial random perturbation for the ice concentration. Figure 3 shows the behaviour of temperature and ice mass concentration on the x,y and x,z midplanes.

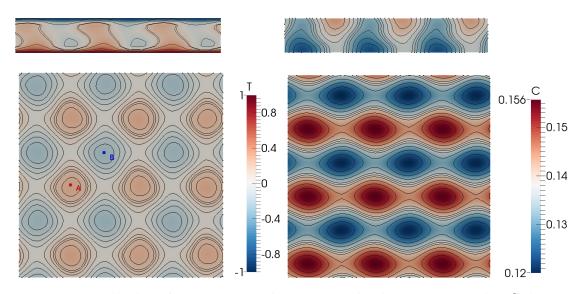


Figure 3: Contours and isolines of temperature, T, left column, and of the ice mass concentration, C, right column, in the x,y midplane, top row, and in the x,z midplane, bottom row, for the ice-water mixture at  $Ra=2.3\times 10^4$ .

Note that on the x,y midplane the distribution of frazil ice concentration follows the trend of the temperature field, showing its maximum values near the zones at lower temperature, whereas the behaviour of frazil ice concentration on the x,z midplane highlights the effects of the transport phenomena due to the  $U_x$  and  $U_y$  velocity components. The velocity fields on the x,y and x,z midplanes are shown in Figure 4, for each components. In Figure 5 we present the temperature and ice concentration profiles, evaluated along two different vertical lines, A, and B. The A,B lines are located on the x,z plane as shown in Figure 3, left plot.

Starting from the numerical solution obtained for the water-ice mixture, an initial uniform salinity distribution has then been imposed on the entire computational domain. The initial salinity field has been set equal to the reference value  $S_0=34.5~psu$ , whereas the boundary condition for salinity at top and bottom walls are zero-gradient. The salt diffusivity and the expansion coefficient are  $\alpha_s=0.7\times 10^{-9}\,[m^2/s]$  and  $\beta_s=7.86\times 10^{-4}\,[1/psu]$ , respectively.

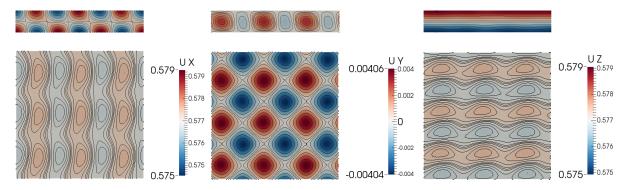


Figure 4: Contours and isolines of  $U_x$ , left column,  $U_y$ , middle column, and  $U_z$ , right column, in the x, y midplane, top row, and in the x, z midplane, bottom row, for the ice-water mixture at  $Ra = 2.3 \times 10^4$ .

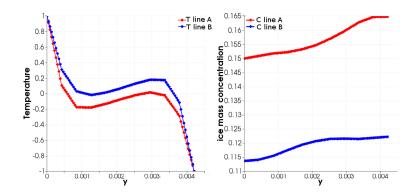


Figure 5: Temperature, left column, and ice mass concentration, right column, profiles along two different vertical lines A, and B, located on the x, z plane as in Figure 3, left plot.

In order to take into account the variation of the freezing temperature due to salinity and width, we define  $T_f = T_{f_0} + ah + a_s (S - S_0)$ , where a and  $a_s$  are the coefficients describing the decrease of  $T_f$  with the width, h, and salinity, respectively, and  $T_{f_0}$  denotes the freezing temperature of the salted water. The simulation has been performed using  $a = 7.61 \times 10^{-4} \, [K/m]$ ,  $a_s = -0.0573 [K]$ , and  $T_{f_0} = 271.17 [K]$ . Here we report the numerical results obtained after about 30 hours of simulated time. Figure 6 shows the behaviour of temperature, ice mass concentration and salinity, on the x, y and x, z midplanes, whereas Figure 7 shows the velocity fields on the x, y and x, z midplanes, for each component. We observe from Figures 6 and 7, that on the x, y midplane the larger values of salinity and frazil ice concentration occur close to the top boundary, where temperature shows its minimum values, conversely the salinity and ice concentration reach their minimum values near to the bottom boundary, where the temperature increases. The behaviour of the salinity and the frazil-ice concentration on the x, z midplane highlights the dependence of the salinity on the temperature distribution, and the effects of the velocity field on the transport of ice particles. In Figure 8 we present the temperature, ice mass concentration, and salinity profiles, evaluated along two different vertical lines, C and D. The C, D lines are located on the x, z plane as shown in Figure 6, middle plot.

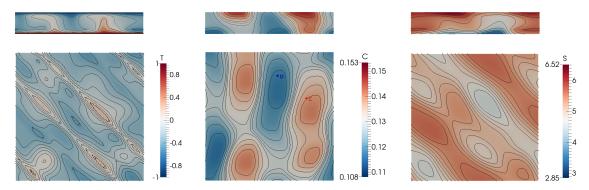


Figure 6: Contours and isolines of temperature, T, left column, ice mass concentration, C, middle column, and salinity, S, right column, in the x,y midplane, top row, and in the x,z midplane, bottom row, for the ice-water-salt mixture at  $Ra = 2.3 \times 10^4$ .

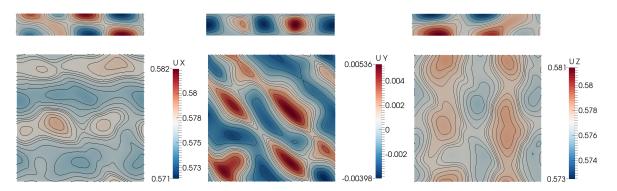


Figure 7: Contours and isolines of  $U_x$ , left column,  $U_y$ , middle column, and  $U_z$ , right column, in the x, y midplane, top row, and in the x, z midplane, bottom row, for the ice-water-salt mixture at  $Ra = 2.3 \times 10^4$ .

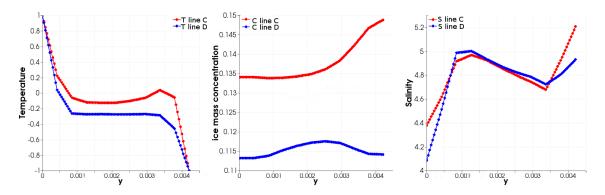


Figure 8: Temperature, left column, ice mass concentration, middle column, and salinity, right column, profiles along two different vertical lines C, and D, located on the x, z plane as in Figure 6, middle plot.

A more comprehensive representation of the convective structures is given in Figure 9, in which we present the three-dimensional contours and isolines of temperature, ice mass concentration and salinity. The isolines are reported on each lateral boundary and on the x,z midplane for y=D/2.

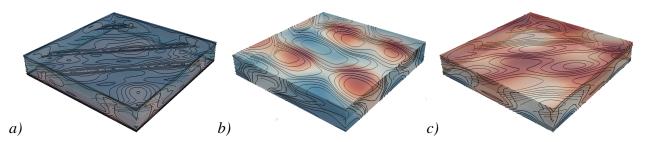


Figure 9: Contours and isolines of temperature, T, a), ice mass concentration, C, b), and salinity, S, c), for the ice-water-salt mixture at  $Ra = 2.3 \times 10^4$ .

#### **6 CONCLUSION AND FUTURE DEVELOPMENTS**

The aim of this work was to improve the predictive capability of the numerical models currently available for the simulation of ice production in seawater, by means of the development of a sophisticated multiphase numerical model able to describe all the stages of ice production, overcoming the limitation of previous attempts, mainly based on the Boussinesq approximation.

We proposed a multiphase model that consider the mixture ice-seawater as a dense compressible fluid, and we modelled the behaviour of seawater density by means of an equation of state, that links density to temperature, pressure and salinity. In order to reproduce the interaction phenomena occurring between phases, we have included in the momentum equations additional terms, derived from the comprehensive modelling approach adopted for the simulation of multiphase flows of industrial interest. A low-Mach number asymptotic analysis has been performed to investigate the behaviour of the multiphase equations in the incompressible limit.

As an initial step of our study, we developed a finite volume numerical solver, by means of the OpenFOAM library, able to reproduce the behaviour of the initial stage of ice formation, according to the Boussinesq approximation. The solver is based on an approximate implicit projection method, according to the colocated version proposed in [4]. The performance of the solver has been assessed by means of the resolution of a Rayleigh-Bénard convection problem, for water and for the mixture ice-seawater. The numerical results obtained for water have been compared with those obtained with a finite difference numerical code.

Ongoing work is focused on the development of an advanced finite volume multiphase solver, for incompressible flows with variable density effects, according to the proposed multiphase approach. We expect that our multiphase model, coupled with the finite volume discretization, could provide an efficient and accurate numerical prediction of all the complex phenomena characterizing the ice production.

#### Acknowledgements

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#### Appendix A Lagrangian derivative of the zero-Mach number equation of state

Here we present the details of the evaluation of the Lagrangian derivative of the seawater equation of state at order  $O\left(M_{\infty}^{0}\right)$ , used for the derivation of the divergence constraint for the water velocity, Equation 41.

The zero-Mach number equation for the seawater density is given by

$$\rho_{w}^{(0)} = D_{r}^{*} \left( D_{r}^{(0)} p^{(0)} \right) + E_{r}^{*} E_{r}^{(0)}, \tag{64}$$

where the coefficients are defined as

$$D_r^* = \frac{D_{r_{\infty}p_{\infty}}}{\rho_w^{(0)}}, \quad E_r^* = \frac{E_{r_{\infty}}}{\rho_w^{(0)}}, \tag{65}$$

$$D_r = \left[ b_5 S_{\infty} T_{\infty} S^{(0)} T_{W}^{(0)} + b_2 T_{W}^{(0)} T_{\infty} + b_1 \right] / D_{r_{\infty}}$$
(66)

$$E_r = \left[ a_5 S_{\infty} T_{\infty} S^{(0)} T_{w}^{(0)} + a_4 T_{w}^2 T_{\infty}^2 + a_3 S^{(0)} S_{\infty} + a_2 T_{w}^{(0)} T_{\infty} + a_1 + \rho_0 \right] / E_{r_{\infty}}$$
 (67)

As reported in section 2.2, the Lagrangian derivative of  $\rho_w^{(0)}$  can be expressed as

$$\frac{D\rho_{\mathbf{w}}^{(0)}}{Dt} = \frac{\partial \rho_{\mathbf{w}}^{(0)}}{\partial S^{(0)}} \bigg|_{T_{\mathbf{w}}^{(0)}, p^{(0)}} \frac{DS^{(0)}}{Dt} + \frac{\partial \rho_{\mathbf{w}}^{(0)}}{\partial T_{\mathbf{w}}^{(0)}} \bigg|_{S^{(0)}, p^{(0)}} \frac{DT_{\mathbf{w}}^{(0)}}{Dt} + \frac{\partial \rho_{\mathbf{w}}^{(0)}}{\partial p^{(0)}} \bigg|_{T_{\mathbf{w}}^{(0)}, S^{(0)}} \frac{Dp^{(0)}}{Dt}.$$
(68)

The partial derivative can be written as

$$\frac{\partial \rho_{\mathbf{w}}^{(0)}}{\partial S^{(0)}} \bigg|_{T_{\mathbf{w}}^{(0)}, p^{(0)}} = \frac{1}{\rho_{\mathbf{w}}^{(0)}} \left( p_{\infty} p^{(0)} b_{5} S_{\infty} T_{\infty} T_{\mathbf{w}}^{(0)} + a_{5} S_{\infty} T_{\infty} T_{\mathbf{w}}^{(0)} + a_{3} S_{\infty} \right),$$

$$\frac{\partial \rho_{\mathbf{w}}^{(0)}}{\partial T_{\mathbf{w}}^{(0)}} \bigg|_{S^{(0)}, p^{(0)}} = \frac{1}{\rho_{\mathbf{w}}^{(0)}} \left[ p_{\infty} p^{(0)} \left( b_{5} S_{\infty} T_{\infty} S^{(0)} + b_{2} T_{\infty} \right) + a_{5} S_{\infty} T_{\infty} S^{(0)} + 2a_{4} T_{\mathbf{w}} T_{\infty}^{2} + a_{2} T_{\infty} \right],$$

$$\frac{\partial \rho_{\mathbf{w}}^{(0)}}{\partial p^{(0)}} \bigg|_{T_{\mathbf{w}}^{(0)}, S^{(0)}} = \frac{p_{\infty}}{\rho_{\mathbf{w}}^{(0)}} \left( b_{5} S_{\infty} T_{\infty} S^{(0)} T_{\mathbf{w}}^{(0)} - b_{2} T_{\mathbf{w}}^{(0)} T_{\infty} + b_{1} \right).$$

and the Lagrangian derivative  $\frac{DS^{(0)}}{Dt}$  and  $\frac{DT_W^{(0)}}{Dt}$ , can be derived from the zero-Mach number temperature and salinity equations, respectively, as

$$\frac{DS^{(0)}}{Dt} = \frac{1}{\left(1 - \phi_I^{(0)}\right)} \left[ \frac{\partial}{\partial x_i} \left( \left(1 - \phi_I^{(0)}\right) \frac{1}{ScRe_{\infty}} \frac{\partial S^{(0)}}{\partial x_i} \right) + S_{sal}^{(0)} - S^{(0)} \left( \frac{\partial}{\partial t} \left(1 - \phi_I^{(0)}\right) + \frac{\partial}{\partial x_i} \left(1 - \phi_I^{(0)}\right) u_i^{(0)} \right) \right] \qquad (69)$$

$$\frac{DT_W^{(0)}}{Dt} = \frac{1}{\left(1 - \phi_I^{(0)}\right)} \left[ \frac{t^* \nu}{L^2} \frac{\partial}{\partial x_i} \left[ \left(1 - \phi_I\right) \frac{1}{Pr} \frac{\partial T_W^{(0)}}{\partial x_i} \right] + \phi_I^{(0)} t^* \lambda_t^{(0)} \left(T_f - T_W^{(0)}\right) + S_T^{(0)} - T_W^{(0)} \left( \frac{\partial}{\partial t} \left(1 - \phi_I^{(0)}\right) + \frac{\partial}{\partial x_i} \left(1 - \phi_I^{(0)} u_i^{(0)}\right) \right) \right] \qquad (70)$$

In order to evaluate the Lagrangian derivative of pressure at zero-order,  $Dp^{(0)}/Dt$ , we consider the momentum equation at the leading order  $O\left(M_{\infty}^{-2}\right)$ . Since  $p^{(0)}$  represent the hydrostatic pressure, for which  $\partial p^{(0)}/\partial z = -\rho_0 g$ , see Equation 35, and considering  $\partial p^{(0)}/\partial t = 0$ , the Lagrangian derivative of the seawater density at order  $O\left(M_{\infty}^{0}\right)$ , can then be rewritten as

$$\frac{D\rho_{w}^{(0)}}{Dt} = \frac{1}{\rho_{w}^{(0)} \left(1 - \phi_{I}^{(0)}\right)} \left(p_{\infty} p^{(0)} b_{5} S_{\infty} T_{\infty} T_{w}^{(0)} + a_{5} S_{\infty} T_{\infty} T_{w}^{(0)} + a_{3} S_{\infty}\right) \left[\frac{\partial}{\partial x_{i}} \left(1 - \phi_{I}^{(0)}\right) \frac{1}{ScRe_{\infty}} \frac{\partial S^{(0)}}{\partial x_{i}}\right) + S_{sal}^{(0)} - S^{(0)} \left(\frac{\partial}{\partial t} \left(1 - \phi_{I}^{(0)}\right) + \frac{\partial}{\partial x_{i}} \left(1 - \phi_{I}^{(0)}\right) u_{i}^{(0)}\right)\right] + \left(b_{5} S_{\infty} T_{\infty} S^{(0)} T_{w}^{(0)} - b_{2} T_{w}^{(0)} T_{\infty} + b_{1}\right) \left[\frac{t^{*} \nu}{L^{2}} \frac{\partial}{\partial x_{i}} \left[\left(1 - \phi_{I}\right) \frac{1}{Pr} \frac{\partial T_{w}^{(0)}}{\partial x_{i}}\right] + \phi_{I}^{(0)} t^{*} \lambda_{t}^{(0)} \left(T_{f} - T_{w}^{(0)}\right) + S_{T}^{(0)} - T_{w}^{(0)} \left(\frac{\partial}{\partial t} \left(1 - \phi_{I}^{(0)}\right) + \frac{\partial}{\partial x_{i}} \left(1 - \phi_{I}^{(0)}\right) u_{i}^{(0)}\right)\right] - \frac{p_{\infty}}{\rho_{w}^{(0)}} \left(b_{5} S_{\infty} T_{\infty} S^{(0)} T_{w}^{(0)} - b_{2} T_{w}^{(0)} T_{\infty} + b_{1}\right) u_{i}^{(0)} \rho_{0} g. \tag{71}$$

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